



Lauer Implementation of Biomass Pyrolysis in Austria – Investigation of Possibilities



Serio Pyrolysis Research at Advanced Fuel Research, Inc. (AFR) on page 13



ThermoNet

ThermoNet comprising PyNe (for biomass pyrolysis) and GasNet (for biomass gasification) had its kick-off meeting in Helsinki at the end of June 2001. PyNe continues to be sponsored by the EC through DG TREN and the Energie programme and by IEA Bioenergy. GasNet will provide an analogous network through Harrie Knoef of BTG in the Netherlands.

The photograph shows Harrie Knoef (leader of GasNet), Kyriakos Maniatis, the EC Project Officer and IEA Bioenergy Executive Committee Vice Chairman, and Tony Bridgwater (leader of PyNe). The focus of PyNe will be based on Technical Topics that are described on pages 7, 8 and 9.







Proceedings from the PITBC Conference now available.

For details of the contents and how to order contact Claire Humphreys or Julie Ellen. For contact details see inside cover.

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In memory of Professor Antonie Adrianus Cornelis Maria (Ton) Beenackers

It is with great sadness and regret that we have to report the death of Ton Beenackers who passed away on 19th April 2001 after a very short illness.

Ton was known to the whole bio-energy community as an enthusiastic and highly competent chemical engineer with a particular interest in thermal gasification. He was closely associated with the EC RD&D programmes for over 20 years and actively contributed to their evolution through both evaluation and definition of new programmes, as well as through active participation in projects. His most recent major contribution was as Chairman of the Technical Programme Committee for the First World Biomass Conference in Sevilla in June 2000, during which he was awarded the Linneborn Prize for his contribution to bio-energy. More recently he acted as Conference Rapporteur for the Progress in Thermochemical Biomass Conversion Conference in Tyrol, September 2000 and had been actively working on the next European Energy from Biomass Conference to be held in Amsterdam in 2002.

Between these commitments he was a dedicated professor at the University of Groningen, where he led a substantial team working on a wide range of projects which included some on aspects of biomass gasification. He encouraged students to follow bio-energy, particularly in developing countries where he actively promoted scientific and technical collaboration with a focus on chemical engineering. He had a particular affinity with Indonesia and was looking forward to implementing a number of collaboration activities between the Institute of Technology in Bandung and the Universities of Groningen and Twente.

He was never reticent and everyone will remember his warm, incisive and positive contributions to discussions and debates including his impeccable attention at a personal level.

The scientific community has lost a personable and highly valued colleague who can never be replaced.

Low-temperature pyrolysis of CCA treated wood waste

Summary

Low-temperature pyrolysis of CCA (copper, chrome, arsenic) treated wood waste at between 300 and 450°C, enables the CCA to be concentrated in the char and hence disposed of more effectively. The evaluation of this technique, focused on metal and arsenic behaviour during the pyrolysis process, in order to understand the behaviour of the contaminants and hence derive models and hypotheses, that describe the influence of CCA on the thermal decomposition chemistry and the release of arsenic.



Figure 1: Experimental facility for the pyrloysis of wood chips: downdraft fixed bed reactor with extended gas cleaning system.

Outline of the work

The influence of temperature and residence time of wood particles on the release of Cr, Cu and As and the resulting mass reduction has been studied experimentally (see Figure 1). The influence of CCA has been studied in the kinetically-controlled regime through thermo-gravimetric studies. Mathematical models have been developed that describe the low-temperature pyrolysis of wood waste:

- A complete macro-particle model (combining heat, mass and momentum transfer with chemical kinetics) for the low-temperature pyrolysis of a single dried, untreated wood particle was implemented and validated.
- A kinetic model for the low-temperature pyrolysis of CCA treated wood was derived from the TG results.
- Finally, physical and chemical models for the release of arsenic during lowtemperature pyrolysis were validated.

Conclusions

Low-temperature pyrolysis is a promising and valuable technique to dispose CCA treated wood waste, provided that temperature and residence time are precisely controlled. The conversion, as well as the metal volatilisation, can be calculated by incorporating the actual temperature profile in the kinetic schemes derived for the pyrolysis of CCA treated wood on one hand and for the release of As during pyrolysis of CCA treated wood on the other hand. CCA promotes charcoal production. Chromium and copper do not pose any problems of metal volatilisation at these low temperatures. Arsenic, on the other hand, is the problematic compound. The mechanism responsible for the As release is identified as the reduction of As(V) to As(III), followed by the volatilisation of As(III). Arsenic is probably released as arsenic trioxide (As₄O₆), which is toxic and very difficult to capture. Limiting As release implies minimising this reduction reaction, which means that the As has to remain in pentavalent form and thus the temperature has to be kept low.

The leaching behaviour of As and Cu restricts deposition of char residue in landfill, whereas the presence of Cr poses no problems

from leaching. The recombination and agglomeration of metals during the pyrolysis process (metal agglomerates are indicated in Figure 2) allows a dry separation of the metal-containing char residue, which allows complete metal recycling. In the near future an installation for the total recycling process will be built, tested and evaluated.

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Figure 2: Longitudinal radial sectional view of ray cells in the pyrolysis residue of CCA treated Pinus sylvestris sapwood (400x) with metal agglomerates on the locations 1, 2 and 3.

Fortum

Finnish Consortium Fortum and Vapo Announce Construction Of Pyrolysis Pilot Plant

By Steven Gust, Fortum, Finland



Figure 1: Location of Pilot Plant.

This process interests both Fortum andOVapo Oy because it can convert renewablefeedstocks such as forestry residues andfeedstocks such as forestry residues andother industrial waste wood to a liquid fuel,which can be used to replace fossil fuels.minthe fuels"These fuels will have increasing demandminthe future as countries look to reducetheir net CO2 emissions," Tapio Alvesalo,Vice President of Corporate Technology

The fuel will be used initially, for heating applications by large customers of light fuel oil, such as schools, retirement homes, office complexes and community buildings etc. Power applications are also being developed. The announcement of pilot plant construction is the conclusion of extensive development work by both companies and their partners in the 1990s in the areas of feedstock selection, processing concepts, pyrolysis fuel properties and use.

emphasizes.

Competitiveness of the partnership

Vapo's R&D Director Timo Nyrönen further emphasises the importance of feedstock logistics to the overall success of the project. This includes proper selection of feed materials, collection and natural drying, chipping and transport to the production plant.

"It is the unique combination of Fortum Oil and Gas, as a refinery and chemical process developer and Fortum Power and Heat as a multifuel customer, utilising a wide variety of different boilers that has given the partners the added confidence required to launch a project of this magnitude" adds Tapio Alvesalo.

Commercial size planned for 2004

The size of the pilot plant was carefully selected to ensure easy scale up to commercial sizes based on past experiences of Fortum. This capacity is suitable for the



Figure 2: feedstock preparation under construction.

Fortum together with it's partner Vapo Oy of Finland have announced they will begin pilot production of a liquefied wood fuel, utilizing a proprietary technology. The approximately 3.2 million euro pilot plant with a capacity of 350 kilograms fuel per hour is currently under construction and is scheduled to begin production in the fall of 2001. The process and products will then be further developed and improved with commercialization planned to begin 2003-2004.

development of applications and further fuel property improvements, but is too small for commercial production which will be roughly ten times this size. The pilot plant which is currently under construction, is situated in an existing building (Figure 1) at the Technology Centre of the Porvoo Refinery, in order to take advantage of the local infrastructure and development staff. Figure 2 shows a portion of the biomass preparation equipment under construction.

"If the test production plant operates according to our expectations and we do not encounter major difficulties in the development work, we will be in a position to start the planning for a commercial-size production plant towards the end of 2002, which would be completed in 2004," says Jukka-Pekka Nieminen, Fortum's Project Development Manager.

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By Stefan Czernik, NREL, USA

In the recent years, the priorities of the NREL research in thermochemical conversion biomass have changed from developing/improving the process for generating liquid product, bio-oil, to converting biomass into gaseous fuel and its use in energy generators (engines, micro-turbines, fuel cells).



Figure 1: 8" Fluidised bed reactor reformer flowsheet.



Figure 2: Fluidised bed reactor at NREL.

For over 15 years, NREL has used the vortex (cyclonic) reactor as its primary reactor for thermoconversion of biomass and related feedstocks. Last year, a fluidized bed reactor was added to the NREL Thermochemical Users Facility (TCUF). The reactor is a 1.8 m high cylindrical vessel of 20 cm diameter in the lower (fluidization) zone, expanded to 36 cm diameter in the freeboard section. It is equipped with a perforated gas distribution plate and an internal cyclone to retain entrained bed media (typically sand). The reactor is heated electrically and can operate at temperatures up to 700°C at a throughput of 15-20 kg/h of biomass. The unit usually operates at similar conditions to those optimized for liquid production. However, superheated steam is used as the carrier gas and pyrolysis vapors, before condensation, are thermally cracked in the secondary tubular reactor at 800-850°C. The char particles are then separated from the gas/vapor stream using two cyclones and, occasionally, hot baghouse filter. The tars and steam are removed in a scrubber system. The unit is equipped with on-line monitors of the gas composition (CO, CO_2 , CH_4 , H_2 , O_2), gas chromatographs, and molecular-beam mass spectrometer. Typically, 1-1.1 kg of gas is produced from 1 kg of biomass.

Clean, dry gas of HHV in the range of 17-19 MJ/kg is used as a fuel for a 15 kW commercial engine devised for combustion of natural gas. At the gas flow of 11 kg/h, the engine efficiency was 27% based on HHV and 29% on LHV. With λ (air to fuel ratio) of 1.2 the emissions included 2.5-3 g CO, 0.20-0.25g THC, and 5-10 g NOx for every kWh of the engine output.

Recently, a catalytic steam reformer was coupled to the pyrolysis/gasification system. Similarly to the pyrolyzer, the reformer is also an externally heated fluidized bed reactor that will be used to produce hydrogen from pyrolysis gas and vapors generated in the first stage of the process and to clean the gas from tars.

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RESEARCH

Implementation of Biomass Pyrolysis in Austria – Investigation of Possibilities

By Maximilian Lauer, Joanneum Research, Austria

An Austrian national project investigated and evaluated the possibilities to produce and to use pyrolysis oil as a fuel. The technical and economical aspects and the status of the technology development were reviewed and recommendations for the implementation in Austria were given.

Production of pyrolysis oil, technology, state of development, cost Several processes for the production of

pyrolysis oil are under development. Concerning the use (shipping, storage, use in burners etc.) it can be compared with a mixture of LFO and HFO. In Europe five demonstration plants will be operating in 2002. In Austria the cost for producing pyrolysis oil will range from 24 to 37 EUR/MWh, this is between prices for fossil fuel oils (light fuel oil, heavy fuel oil) in average from May 2000 to May 2001. A sufficient availability of wood as feedstock for pyrolysis is assured in Austria.

Use of pyrolysis oil, technologies, state of development, economics

Pyrolysis oil can be used as a fuel for heating boilers (> 200 kW), low speed Diesel engines and gas turbines. Up to now, no appropriate burner technology is available for small heating boilers. The use in intermediate and big boilers are proven by experimental work in Finland and Sweden; no major problems are expected for the development to the state of the art. Experiments on the use in low speed Diesel engines with CHP were quite successful. In 2002 a demonstration plant will be put into operation in the UK. The use in gas turbines is in the experimental phase; there are plans to start a demonstration plant in the UK in 2002. The economics for the use of pyrolysis oil in heating boilers are guite good compared to the use of fossil fuel oils. Also the competitiveness of using pyrolysis oil in Diesel engines is good. The use in gas turbines is only competitive under specific conditions. In Table 1 the competitiveness as an indicator for the economic situation is given, comparing the use of pyrolysis oil with the use of wood chips both in boilers and in CHP plants. Wood chip boilers are more competitive than pyrolysis oil boilers. But practically the use of wood chip boilers is restricted to the wood processing industry. Pyrolysis oil boilers can be used in all branches of industry. Competition between pyrolysis oil and wood chip boilers has to be considered only in the wood processing industry.

Environment, Health and Safety

Standards for the pyrolysis oil as a product and for shipping and handling do not exist, although in preparation. Compared to the use of fossil fuels a reduction between 59% and 84% of the greenhouse gas emission (depending on the specific application) can be achieved.

Recommendations for the Implementation in Austria

Based on the project results, recommendations for further activities aiming on implementation of pyrolysis technology in Austria are given:

 Realisation of a pilot pyrolysis plant (in the case of positive results of the demonstration plants in Europe).

Pyrolysis Oil	Power	cf	Wood chips	Power	cf
Boilers	0.5 MW	0.98–1.36	Boilers	0.5 MW	1.62
	2 MW	1.03–1.46		2 MW	1.88
	5 MW	1.04–1.48		5 MW	2.01
CHP-plants			CHP-plants		
Diesel	2.4 MWe	0.92–1.22	FB – Gasifier CHP	0.5 MWe	1.08
Gas Turbine *)	20 MWe		Biomass IGCC *)	45 MWe	1.3

Table 1: Competitiveness of the use of pyrolysis oil compared to the use of wood chips (Austria 2001).

- cf: Indicator of the competitiveness (cost relation to conventional energy supply) cf < 1: not competitive cf increases with competitiveness
- *) basis for cost estimation rather unsure
- Realisation of experimental and demonstration plants for heating boilers and Diesel engine CHP.
- Technical development of small scale heating boilers.

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PyNe TECHNICAL TOPICS

A number of Topics have been agreed to form the focus of the technical contributions of PyNe over the next three years. Some are being carried out in co-operation with the associated Network in ThermoNet – GasNet and these are indicated as Joint Topics. In addition, other aspects will be routinely covered such as technology developments and in associated projects such as economic and financial aspects. A summary list is shown below and further details of the PyNe and Joint topics are also provided.

PyNE Topics and Leaders				
Applications for bio-oil Characterisation, analysis, norms & standards Environment, health and safety aspects of bio-oil Slow pyrolysis for charcoal Technical and non technical barriers Technology review Economics and finance	S. Czernik D. Meier and A. Oasmaa P. Girard M. Gronli W. Prins To be covered in an associated ALTENER Project			
Joint Topics and Leaders				
Education, training, information and PR Environment, health & safety – general aspects Gas processing and tar reactivity Country reports	J. Arauzo (PyNe) + G. Neri (GasNet) R. Buehler (GasNet) + P. Girard (PyNe) I. Gulyurtlu (GasNet) + K. Pedersen (PyNe) All members			

PyNe TOPICS

Applications for bio-oil Leader: Stefan Czernik



Objectives

- Review current applications for fast pyrolysis liquids
- Define research needs to enhance and develop the use of bio-oil

Scope

- Application of bio-oil as liquid fuel for boilers, engines and turbines

 e.g. performance, emissions
- Potential of bio-oil as a transport fuel – e.g. upgrading, blending
- Bio-oil as a source of chemicals

 e.g. liquid smoke, adhesives, fertilizers, bio-lime, fine chemicals

Work Plan

- Review of literature on combustion
 of bio-oil list of references
- Analysis of advantages and deficiencies of bio-oil as fuel – Upgrading methods
- Emissions from bio-oil combustion – Can they meet standards?
- Identify new potential applications
 Co-firing, blend, slurries
- Research needs to enhance use

Deliverables

- Reports on fuel and chemicals
- Publications, presentations

Norms, Standards, Characterisation & Analysis Leaders: Dietrich Meier and Anja Oasmaa



Objectives

- Review and update physical and chemical methods
- Review and update properties of oils from demonstration plants
- Formulate recommendations for specifications and classification of bio-oils

Scope

• Methods for testing and analysis

Work Plan

• Review and update methods for analysis and characterisation

- Identify on-line methods
- Identify methods for physical upgrading
- Assess correlation between oil quality and composition
- Recommend handling and analytical procedures
- Propose classification system
- Distribute instructions and standards for analyses

Deliverables

- Report on recommended handling and analytical methods for pyrolysis liquids
- Proposed list of specifications

Environment, Health and Safety Leader: Philippe Girard

Objectives

- Improve knowledge on E.H.S. concerns at
 - 3 levels:
 - Regulations
 - Process emissions
 - Bio oil toxicity

Scope

- Collect and review data and information
 - Carry out toxicity test
- Collection and review of existing regulations (in collaboration

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with GasNet)

Work programme

- Develop and circulate a questionnaire
- Collation of information
- Reporting
- Slow Pyrolysis for Charcoal Leader: Morten Grønli
 - Scope
 - Feedstock:
 - native wood
 - agro residues
 - solid-recovered biofuels
 - Production:
 - pre-processing (size reduction, drying and handling)
 - carbonization processes
 - emissions
 - Utilization:
 - energy (cooking, co-firing, etc.)
 - industry (metal reduction, filtration,
 - activated carbon, etc.)

Work Plan

- Prepare a guestionnaire and compile information on available industrial carbonization processes. Process the information and make a state of the art review
- Prepare a questionnaire and compile information from each member country

- Collect existing emission data (in collaboration with GasNet)
- Develop a proposal to fund a bio-toxicity study

Deliverables

- Set of European/US regulations information data
- Process environmental impact data
- Set of necessary, toxicological and eco-toxicological data for substance notification (ELINCS)
- Data for process optimisation
- Recommendations for safety procedures

collate the information and prepare a report

- Arrange a seminar/workshop
- Distribute information on PyNe Web-site

Deliverables

- Report on available industrial carbonization processes including feedstock pre-processing and emission control systems Report on:
 - charcoal production and processes in each member country
 - import/export figures in each member country
 - charcoal utilization in each member country (metallurgical/cooking/etc.)
 - Report on:
 - future (potential) utilization of charcoal
 - technology improvements and research needed

Technical/Non-Technical Barriers Leader: Wolter Prins



Objectives

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- Identify and monitor barriers
- Assess routes for solution
- Remove the barriers, where possible

Scope

- Technical, such as:
 - Pyrolysis plant and environment interaction
 - Phase stability
 - Solids in oil application related
 - Water, mineral content
 - Acidity
 - Odour
 - Noise
 - Emissions
- Non-technical such as:
- Capitalization
- Requirement for standards
- Requirement for EHS data
- Alternatives, wind, solar, ethanol, fossil
- Feedstock cost and scarcity
- Public perception
- National/local legislation

Work Plan

On a bi-annual basis circulation by mail of a list of barriers and solution. PyNe members can add barriers and routes of solution to the list. This list will be re-circulated amongst the PyNe members and parts of it published in the PyNe newsletter. If desired experts can be contracted to provide some of the most pressing solutions. Dissemination of information by means of a PyNe workshop and through the newsletter and website.

Deliverables

- Bi-annual updated list of technical and non-technical barriers and their status Identification of routes for solution
- Publication and dissemination of results



- Provide industry, researchers and decision makers a state of the art review of technologies for slow pyrolysis
- To identify the need for technology development and new exploitation of charcoal

JOINT TOPICS WITH GasNet

Education, Training, Information & PR Leaders: Jesus Arauzo and Giuseppe Neri (GasNet)



- To promote the use of thermochemical processes, pyrolysis and gasification as a source of energy
- To deliver clear and comprehensive information about processes and installations
- To promote courses and exchange of students

Work Plan

- Information
 - Standard basic information sheets on processes and installations
 - Review of existing
 - thermochemical course
 - List of host institutions
 - Events

- Education
- Targeted courses on specific topicsSummer courses
- Student exchanges school school and school – industry
- Training
- Courses for technical and non-technical people

Deliverables

- List of courses (programmes)
- List of institutions
- Summer courses programme
- Video/CD ROM

Gas processing & tar reactivity Leaders: Karsten Pedersen and Ibrahim Gulyurtlu (GasNet)



Objectives

- Collect information about gas upgrading regarding
- Particle separation
- Aerosols
- Tar characteristics and reactivity
- Process requirements
- Contaminants from waste

Scope

- Different gasification and Pyrolysis processes
- Identification of particles tars and emissions of pollutants with different processes

Work programme

- Review existing information
 Collect new information
- Collect new information
- Organize a workshop/seminar on this particular topic
- Identify needs for further R&DCoordinate information with
- IEA Activities

Deliverables

Provide information for a database for ThermoNet

Environmental Health and Safety (General) Leaders: Philippe Girard and Ruedi Buehler (GasNet)



Objective

 To review all aspects of environment, health and safety that impact on thermal biomass conversion processes

Scope

 Collect and review data and legislation pertaining to gasification and pyrolysis processes and products

Work Programme

- Collect data on gasification and pyrolysis processes in terms of emissions from members of both Networks and any other relevant sources
- Collect data on gasification and pyrolysis products as made and as used from members of both Networks and any other relevant sources
- Compile information on current and proposed legislation that may impact on commercial implementation of thermal conversion processes

 Collate members experiences on EHS aspects of implementation at research development and commercial stages of development

Deliverables

- Report on thermal conversion process emissions
- Report on emission from products as made and in use
- Report on current and planned legislation and its impact on implementation
- Report on practical experiences of plant operation in terms of EHS

Energy



By John Brammer, Bio-Energy Research Group, Aston University, UK



Fuel Oils

Country	Country Heavy Fuel Oil			Heavy Fael Oil Light Fael Oil (Industry)			Light /	sel Oil (Dos	nestic)
	ex-tax	tax	total	ex-tax	tax	total.	ex-tax	tax	total
Austria	119.3**	41,4**	160.7**	157.4**	39.4**	196.8**	297.3	150.3	447.5
Belgium	195.4	0.8	171.4	271.1	13.6	289.5	276.1	74.4	350.5
Canada	1	1 2201	190.5	10000000	1.000	262.8	1.000	1000	Section 2
Denmark	184.5	50.1	234.6	377.5	32.5	410.0	330.1	416.5	745.5
Fieland	183.7	55.1	248.7	286.2	67.3	363.5	286.2	145.1	431.3
France	187.6	17.9	205.4	278.3	80.2	359.3	320.0	145.5	486.1
Germany	183.9	17.7	181.1	288.9	81.1	361.1	288.5	117.3	407.3
Greene	207.2	37.3	244.5	303.3	114.8	415.8	303.1	388.8	490.8
Entand	224.7	13.1	137.8	736.5	47.2	343.8	381.4	38.2	459.7
Italy	133.0	30.2	223.2	337.2	375.6	714.0	337.2	515.5	8.438
Japan	300.1	15.0	315.1	295.3	14.8	301.9	450.B	22.5	473.A
Netherlands	195.5	29.5	228.5		1.	1	334.2	227.6	561.8
Roway	254.6	115.2	370.9	448.2	57.B	504.0	451.5	175.1	6.568
Portugal	231.7	12.0	243.7			1			-
Spain	224.4	12.9	237.A	286.6	78.4	365.2	286.8	136.8	423.6
Sweden		5	4	253.6	12.5	1112.3	300.0	341.0	641.0
Switzertan#	192.0	7.6	189.0	251.3	8.7	276.0	213.5	31.4	325.3
United Kingdom	158.7	43.4	200.1	215.1†	50.71	285.81	284.3	\$7.5	361.8
United States		1 1 1 1	178.7	1.000 Mar	1000	251.5			389.0



Average prices over full year, except † part year only, * 1999, ** 1998

All liquid fuel prices in Euro/1000l

All gas and electricity prices in Euro/100kWh (or c/kWh), gas on GCV basis All currency conversions based on exchange rates only 1 Euro = 0.925 US\$, 1.955 DM Principal source: IEA Energy Prices and Taxes, 1st Quarter 2001 (ISBN 92-64-19069-4) Brazil omitted as no data available





Prices & Taxes 2000

Country	Country Diesel (Commercial)		Diesel	Diesel (Nan-commercial)			Gasoline		
	ex-tax	tax	total.	ex-tax	tax	total.	ex-bax	tax	total
Austria	357.7	266.6	140.3	357.B	417.6	775.6	365.0	569.2	138.2
Belgium	362.6	289.0	#51.6	378.5	429.1	807.7	358.0	685,7	1044.7
Casada	333,4	162.3	495.B	10.62	5. 36 Martin	Construction of the	367.6	229.3	597.0
Denmark	615.1	343.4	758.5	414.7	532.8	147.6	381.4	744.3	1135.7
Finland	391.4	302.8	114.4	381.4	455 Å	847.2	361.5	761.0	1130.5
France	320.6	384.1	704.9	371.5	524.4	A46.0	332.2	762.3	1014.4
Germany	311.3	377.0	\$55.3	211.3	487.0	798.3	311.3	700.0	1001.3
Greece	225.3	245.4	\$71.7	375.3	248.4	174.7	370.1	410.8	761.0
Exitand	317.5	317.4	185.3	375.5	487.8	636.3	315.4	\$24.7	880.2
Italy	359.2	L 285	741.5	359.2	530.5	869.7	380.3	700.3	1060.6
Japan	235.5	341.0	\$40.8	485.4	363.0	841.5	477.4	590.7	1068.0
Netherlands	385.0	350.4	719.4	365.0	475.1	845.1	392.0	767.3	1159.3
Roway	440.5	548.1	\$58.9	440.8	775.8	1216.4	406.8	891.7	1298.5
Portugal	314.0	292,4	106.4	311.5	339.7	#51.1	437.7	427.2	864.9
Spain	326.8	268.8	595.7	326.6	364.2	\$91.0	333.7	483.5	A16.8
Sweden	452.8	345.6	758.4	452.6	545.2	1188.0	370.5	753.1	1124.0
Switzertand	256.5	493,1	780.1	358.7	581.7	120.3	358.1	540.5	6.676.0
United Kingdom	340.2	791.6	1131.8	340.2	\$69.5	1329.7	320.6	\$85.2	1306.8
United States	1	1	1.000	231.2	125.5	422.7	373.0	110.3	483.2







Gas

Country	Nata	ral Gas (Inda	sty)	Natural Gas (Domestic)		
	ex-tax	tax	total.	ex-tax	tax	total
Austria	1.19**	· · · · · ·	1.15**	1.35	68.0	3.84
Belgiam				2.43**	0.67**	3.16**
Canada	2	3	DAC	11666	30 A. A.	1.71
Denmark	8	Concernant State	A Street Sec.	3.38	3.45	1.54
Fisland	1.05	0.15	1.22	1.05	0.43	1.48
France			1.56	2.25	0.48	3.23
Germany	1.18**	0.18**	1.37**	7.57**	0.60**	3.12**
Greece	7,47*	0.70*	2.87*	1.771	0.147	1.91
Entand	1.35	A	1.35	16.5	0.38	3.21
Italy	1.18**	0.13**	1.32**	2.75*	2.34*	5.34*
3apan	3.51*	0.18*	3.79*	11.20*	0.55*	11.76*
Notherlands.	1.48	0.07	1.55	2.16	1.18	3.34
Roway	1		1			-
Pertugal	-	· · · · · ·				
Spain	1.63		1.63	3.88	0.69	4.57
Sweden	-	S	- C			1
Switzertand	2.05	50.0	2.07	3.54	0.29	EA.E
United Kingdom	0.901	A	0.90*	2.53	0.13	2,72
United States	1.55	3	1.58		1	2.86



Electricity

Country	Elect	ricity (Indu	stry)	Electricity (Domestic)		
	ex-tax	tax	total	ex-tax	tax	total
Austria	7.03*+		7.08**	9.48	3.65	13.12
Belgium	4.68**		4.55++	12.08**	2.70**	14.79**
Canada	8	1 and the little	17201-075	- 200 - 1	10.222.07	1002000000
Denmark	5.16	1.05	5.24	8.55	12.79	21.34
Finland	3.74	0.43	4.17	6.18	2.22	6.41
France	4.18**	1	4.15**	8.84**	2.71**	11.55**
Germany	6,32*	3	5.32*	32,24*	1.94*	14.17*
Greece	4.60*		4.10	7.651	0.617	8.267
Excland	5.29	1.000	5.25	9,74	1.71	10.95
Italy	8.15	1.47	3,82	11.29	3.35	14.64
Japan	15.04*	1.22*	15.25*	22.57*	1.60*	74.25*
Netherlands	5.94	0.24	8.17	9.A3	4.34	14.17
Roway			1.00	3.94	2.20	1.17
Partugal	7.25		7.25	12.40	0.62	13.08
Spain	6.31*	0.25*	5.21*	10.35*	2.41*	13,39*
Sweden	*		4 1			1
Switzertand	0.91	1	4.55	11.30	0.64	12.03
United Kingdom	6.071	1	\$,07*	10.87	0.55	11.53
United States	11	1	1		1.000	1000000





Pyrolysis Research at Advanced Fuel Research, Inc. (AFR)

By Michael A. Serio, AFR, East Hartford, CT USA

AFR has been involved for several years in R&D on the pyrolysis-based conversion of biomass into fuels, chemicals and materials. Much of this work has been sponsored by the U.S. Government, in particular the Department of Energy (DOE), the National Science Foundation (NSF), the Environmental Protection Agency (EPA), the U.S. Department of Agriculture (USDA) and the National Aeronautics and Space Administration (NASA). In addition, significant biomass R&D work has been carried out for private companies and institutions.



Figure 1: Sequential FT-IR spectra of xylan sample from TG-FTIR analysis at 30°C/min.

A primary investigative tool is a thermogravimetric analyzer equipped with FT-IR analysis of evolved gases (TG-FTIR). While TG-FTIR systems are available from several manufacturers, the system used at AFR was developed in-house with the collaboration of Bomem, Inc., an FT-IR spectrometer company. It is designed to permit analysis of the heavy tars (liquids) that form from the pyrolysis of biomass materials, in addition to the light gases [1]. A stack plot of FT-IR spectra collected from pyrolysis of a sample of xylan in the TG-FTIR apparatus is shown in Figure 1.

AFR

Figure 2 (see page 14) shows a comparison of quantitative evolution rate data for major pyrolysis species from the TG-FTIR for samples of cellulose, xylan and an organsolv lignin. These types of data are usually collected at multiple heating rates and used to build pyrolysis models based on the methodology used in AFR's Functional-Group. Depolymerization, Vaporization, Crosslinking (FG-DVC) model [2]. The data in Figure 2 clearly show the differences in the pyrolysis behavior of the different feedstocks. For typical biomass samples, quantitative data are routinely obtained on nearly 20 volatile species, including tars, H₂O, CO,CO₂, COS, SO₂, CH₄, C₂H₄, HCN, NH₃, acetic acid, acetaldehyde, formic acid, formaldehyde, methanol, phenol, acetone, and levoglucosan.

Many different types of biomass materials and waste products have been studied. These include the pyrolysis of lignin to produce chemicals [3], pyrolysis of waste tires to produce activated carbon and carbon black [4], and pyrolysis of plant biomass materials to produce fuel gases, chemicals and materials (activated carbon) [2]. A current NASA sponsored study is developing a prototype pyrolyzer for recycling of mixed solid waste streams in space [5]. The equipment is shown in Figure 3 (see page 14). AFR is constantly expanding its biomass pyrolysis database with the purpose of providing kinetic and composition inputs to the biomass pyrolysis model. The kinetic data collected at low heating rates, where product resolution and quantification are relatively easy, is used in the model to obtain predictions for high heating rate pyrolysis.

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Figure 2: Comparision of TG-FTIR pyrolysis data for cellulose (squares), hemicellulose (xylan, diamonds), and ALC lignin (circles) at 30°C/min.

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Figure 3: Picture of inlet side of NASA prototype pyrolyser.



Energie Aus Holz 2001

Venue:	Straubing, Germany
Date:	4-7 October 2001 Contact:
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18th World Energy Congress: Energy Markets: The Challenges of the **New Millennium**

Venue:	Buenos Aires, Argentina
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Contact:	18th WEC
	c/o Congresos Internationales SA
	Moreno 584 – Piso 9
	1091 Buenos Aires, Argentina
Tel:	+54 1 4342 3216/4342 3283
Fax:	+54 1 331 0223/334 38111
Email:	18th-wec@congresosint.com.ar

Renewable Energy Indonesia 2001

Venue:	Jakarta's International Exhibition
	Centre, Kemayoran
Date:	7-10 November 2001
Contact:	Stephen Luff
	Overseas Exhibition Services Ltd
	11 Manchester Square
	London
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Tel:	+44 207 862 2090
Fax:	+44 207 862 2098
Email:	indonesia@montnet.com
Website:	www.montnet.com

2nd Annual European Renewables 2001 Summit

Venue:	Brussels, Belgium
Date:	20-21 November 2001
Contact:	Inbal Osmo
Tel:	+44 (0)207 704 6161
Fax:	+44 (0)207 354 9590
Email:	iosmo@thecwcgroup.com
Website:	www.thecwcaroup.com

Conferencia Cientifica internaacional MEDIO AMBIENTE SIGLO XXI

Venue:	Santa Clara, Cub
Date:	20-24 November 2001
Contact:	Ing. Pedro Casanova Treto
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Diary of Events

Information compiled by Claire Humphreys, Aston University, UK

International Conference on Energy and Quality of Life Policy Directions in the New Millennium and Symposium on Lighting Baroda, India Venue: 29-30 November and Date: 1 December 2001 Contact: Professor Rachel George or Ms Z Marina **Conference Secretariat** Technical Backup Support Unit NPIC Home Management Dept, Faculty of ome Science The Maharaja Sayajirao University of Baroda Vadodara 390 002 India Tel: +91 265 794864; 795060; 786429 Fax: +91 265 794864 **Fmail** rachel_george1@rediffmail.com

6th European Conference on Industrial **Furnaces and Boilers**

Estoril, Lisbon, Portugal Venue: Date: 2-5 April 2002 Professor Albino Reis Contact. Rua Gago Coutinho, 185-187 4435-034 Rio Tinto Portugal +351 22 973 4624; 0747 +351 22 973 0746 Email: conference@infub.pt Website: www.infub.pt

BIOS ENERGIE 2002

Tel:

Fax:

Venue Lons le Saunier, France 4-7 April 2002 Date: Contact: Francçis Bornschein or Cécile Pierron BP 149 28 Boulevard Gambetta F-39004 LONS LE SAUNIER cedex, France Tel: +33 384 47 8100 +33 384 47 8119 Fax: salons@itebe.org Email: Website: www.itebe.org

Technibois Energie 2002

Venue: Québec, Canada 2-4 May 2002 Date: Contact: Rolande Gauvin **GESTION TB Inc** C.P. 1010 CAN-G6P 8Y1 Victoria (Québec), Canada Tel: +1 418 845 8247 +1 418 845 8576 Fax: Email: gesttb@videotron.ca Website: www.technibois.com

Sustainable Development of Energy, Water and Environment Systems

	· · · · · · · · · · · · · · · · · · ·
Venue:	Dubrovnik, Croatia
Date:	2-7 June 2002
Contact:	2002 Dubrovnik Conference
	Energetika Marketing
	Sokolska 25
	HR-10000 Zagreb, Croatia
Tel:	+358 1 3771 256
Fax:	+358 1 3772 429
Email:	dubrovnik2002@ege.hr
	-

12th European conference and Technology Exhibition on Biomass for Energy, **Industry and Climate Protection**

Venue: Amsterdam, Netherlands Date: 17-21 June 2002 Contact: ETA-Florence Piazza Savonarola, 10. I-50132 Florence +39 055 500 2174 Tel +39 055 57 3425 Fax: Email: eta.fi@etaflorence.it Website: www.etaflorence.it OR WIP-Munich Contact: Sylvensteinstr., 2 D-81369 Munich +49 89 720 1235 Tel: +49 89 720 1291 Fax: Email: wip@wip-munich.de Website: www.wip-munich.de

ISREE-8 Conference

Venue: Orlando, Florida Date: 4-8 August 2002 www.fsec.ucf.edu/ed/iasee Website:

Waste Management 2002

Date:

Tel:

Fax:

Venue: Cadiz, Spain 4-6 September 2002 Gabriella Cossutta Contact: **Conference** Secretariat Waste Management 2002 Wessex Institute of Technology Ashurst Lodge, Ashurst Southampton, SO40 7AA, UK +44 (0) 238 029 3223 +44 (0) 238 029 2853 Email: enquiries@wessex.ac.uk www.wessex.ac.uk/conference Website: /2002/waste02/

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PyNe Group in Helsinki, Finland, June 2001.



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